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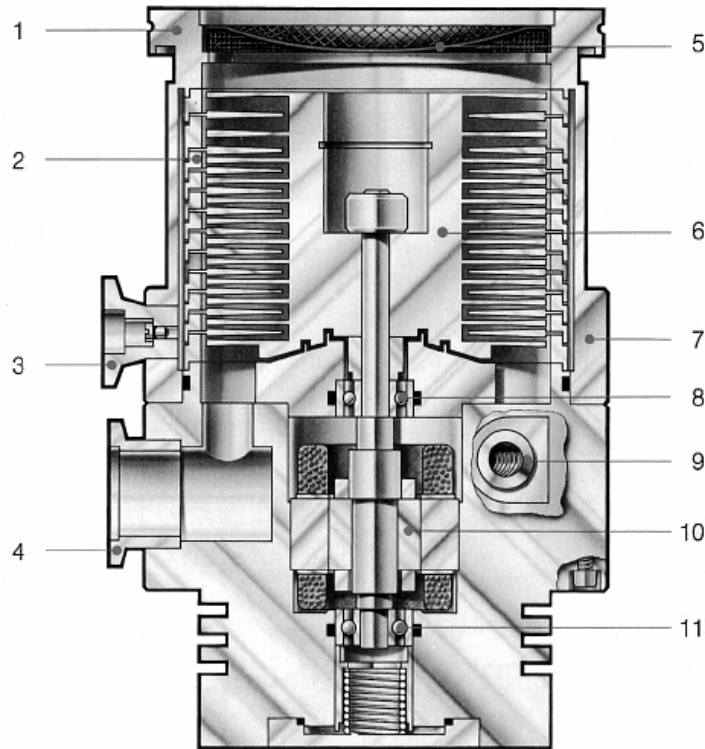
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***Analytical Modeling  
of Turbomolecular Pumps and Roots Blowers***

**Gerhard Voss**

**Oerlikon Leybold Vacuum, Cologne, Germany**

# Classical Turbomolecular Pump



- |                              |                   |                       |
|------------------------------|-------------------|-----------------------|
| 1 Hochvakuumanschlußflansch; | 5 Splitterschutz; | 9 Kühlwasseranschluß; |
| 2 Stator-Paket;              | 6 Rotor;          | 10 3-Phasen-Motor;    |
| 3 Belüftungsanschlußflansch; | 7 Pumpengehäuse;  | 11 Kugellager         |
| 4 Vorvakuumanschlußflansch;  | 8 Kugellager;     |                       |

## How to calculate the compression curve of a classical turbomolecular pump ?

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Classical turbomolecular pump (TMP) = TMP without compound stage

### Analytical model:

TMP in one dimension:

$x = 0$  : High-vacuum flange (= inlet flange)

$x = L$  : Foreline port; L is taken as the effective length of the TMP

## Basic assumptions

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Ansatz:

$$Q = Q_{\max} - Q_{\text{bs}}$$

Net gas throughput = Maximum gas throughput in forward direction – Backstreaming

$$p_1 \cdot S_{\max} = p \cdot S_{\max} - r \cdot (1/h_v) \cdot (p + p_2) \cdot (dp/dx)$$

$h_v$  : Dynamic viscosity in the range of viscous flow

$p_2$  : Empirical parameter (depends on the geometry of the TMP) {  $p_2 = p_2(Q)$  }

## Differential equation

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Differential equation:  $(p + p_2) \cdot (dp/dx) = (p - p_1) \cdot (C_2/L)$

Boundary condition:  $p(x = L) = p_{FV}$  (= foreline pressure)

- x** : Position inside the TMP  $\{ 0 \leq x \leq L \}$
- p** : Pressure inside the TMP  $\{ p(x = 0) = p_{HV} \leq p = p(x) \leq p_{FV} = p(x = L) \}$
- p<sub>1</sub>** : Lowest high-vacuum pressure which can be attained with the TMP  
at the prescribed gas throughput Q  $\{ p_1 = p_1(Q) \}$
- C<sub>2</sub>** :  $C_2 = h_v \cdot S_{max} \cdot L/r$
- h<sub>v</sub>** : Dynamic viscosity in the range of viscous flow
- S<sub>max</sub>** : Maximum pumping speed at the inlet flange  
at the prescribed gas throughput Q  $\{ S_{max} = Q/p_1 = S(p_1) \}$
- L** : Effective length of the TMP
- r** : Backstreaming coefficient  $\{ r = r(Q) \}$

## Solution of the differential equation

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$$p = p_1 + (p_{FV} - p_1) \cdot \exp(b \cdot (p_{FV} - p - C_2 \cdot [1 - x/L]))$$

$$b = 1/(p_1 + p_2)$$

$$C_2 = h_v \cdot S_{max} \cdot L/r$$

$p_2$  and  $C_2$  are the crucial parameters of the model.

$$p(x=0) = p_{HV} = p_1 + (p_{FV} - p_1) \cdot \exp(b \cdot (p_{FV} - p_{HV} - C_2))$$

Ⓐ solve for the high-vacuum pressure  $p_{HV}$  numerically or

Ⓐ use an analytical approximation, if  $p_{HV} \ll p_{FV}$ :

$$p_{HV} = p_1 + (p_{FV} - p_1) \cdot \exp(b \cdot (p_{FV} - C_2))$$

The **compression curve  $K(p_{FV})$  of the TMP** is given by

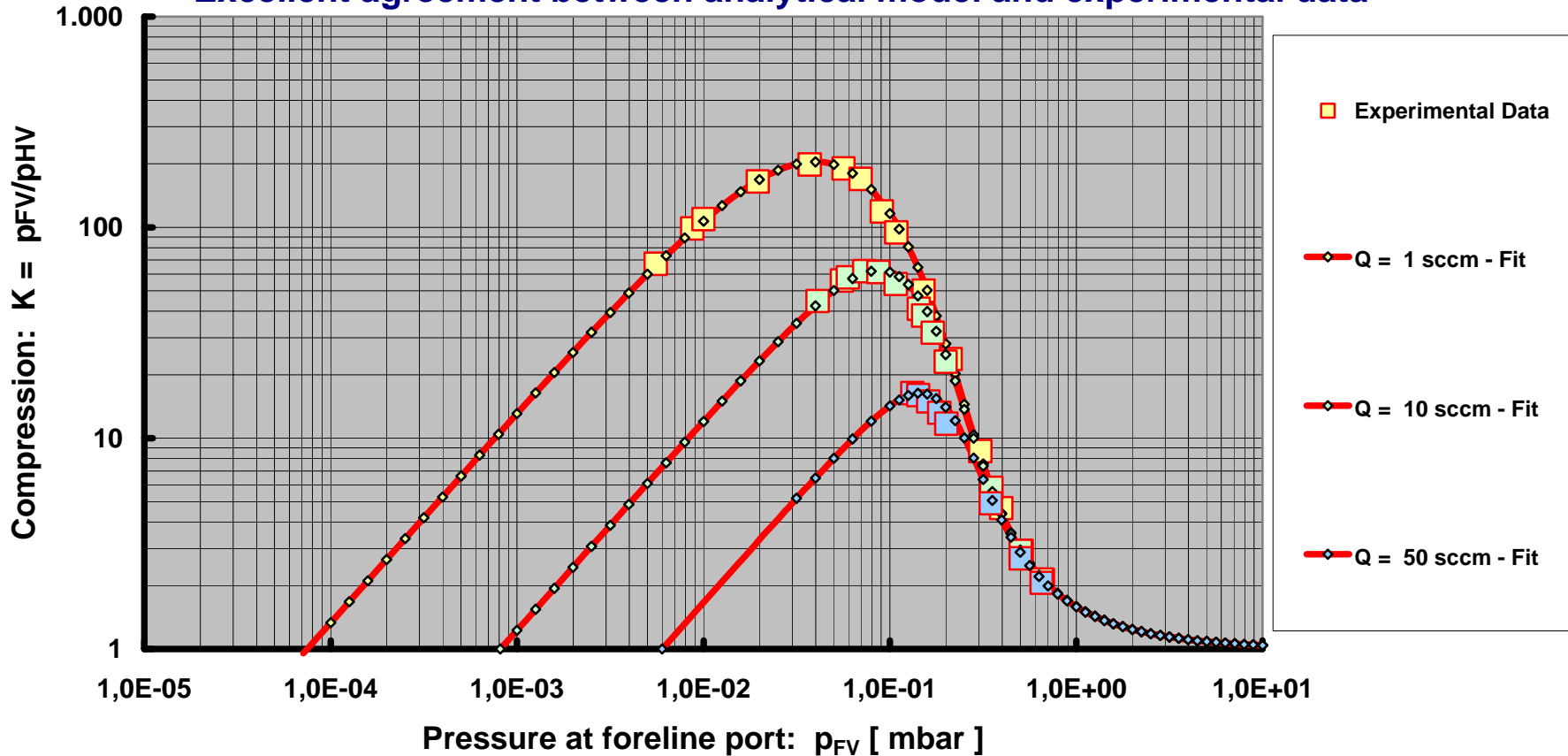
$$K(p_{FV}) = p_{FV} / p_{HV}$$

**TMP without compound stage (100 ISO-K; Rotational speed: 750 Hz)**

**Compression - Hydrogen**

(  $p_2 = 6,2 \times 10^{-2}$  mbar,  $C_2 = 0,4$  mbar )

**Excellent agreement between analytical model and experimental data**



## Intuition

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The analysis of the compression curves leads to the following intuition:

**The parameters  $p_2$  and  $C_2$  are constants and do not depend on throughput, provided the throughput  $Q$  is less than 100 sccm.**

**Consequently,**

$$S_{\max}/r = C_2/(h_v \cdot L)$$

**does not depend on throughput and is a constant.**



## Zero throughput compression

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$$Q = 0 \quad \text{p}_1 = 0$$

$$\text{p}_{\text{HV}} = \text{p}_{\text{FV}} \cdot \exp(-(\text{p}_{\text{FV}} - \text{p}_{\text{HV}} - C_2)/p_2)$$

$$K_0(\text{p}_{\text{FV}}) = \text{p}_{\text{FV}}/\text{p}_{\text{HV}} = \exp(-(\text{p}_{\text{FV}} - \text{p}_{\text{HV}} - C_2)/p_2)$$

In the limit  $\text{p}_{\text{HV}} \ll \text{p}_{\text{FV}} \ll C_2$  we obtain for the zero throughput compression of the TMP:

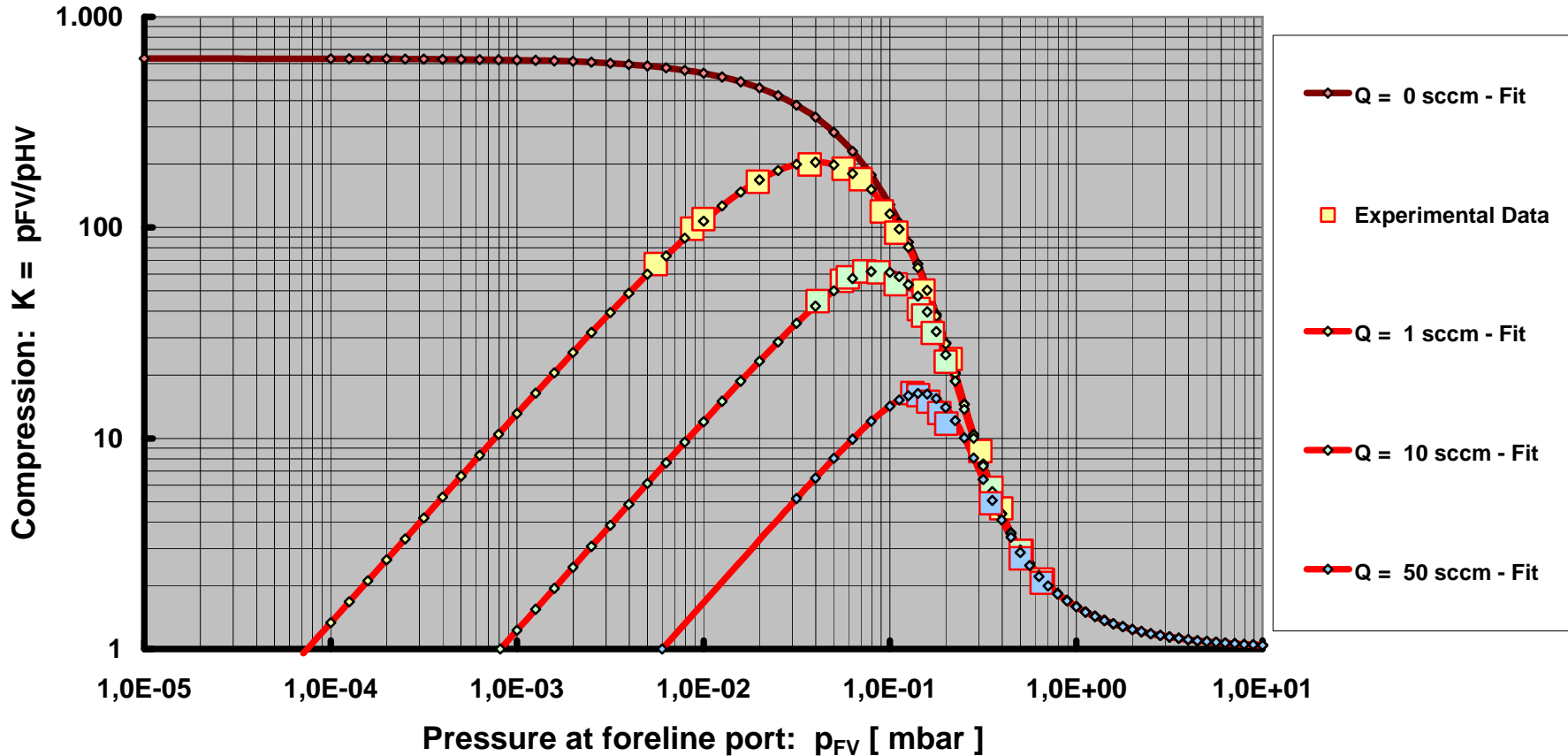
$$K_0 \approx k_0 = \exp(C_2/p_2)$$

**Hypothesis: The zero throughput compression curve of a TMP can be derived from a compression curve for finite throughput, e.g.  $Q = 1$  sccm. This can be achieved by using the parameters  $p_2$  and  $C_2$  determined from the  $Q = 1$  sccm-compression curve to calculate the zero throughput compression curve.**

**TMP without compound stage (100 ISO-K; Rotational speed: 750 Hz)**

**Compression - Hydrogen**

(  $p_2 = 6,2 \times 10^{-2}$  mbar,  $C_2 = 0,4$  mbar,  $k_0 = \exp(C_2/p_2) = 634$  )

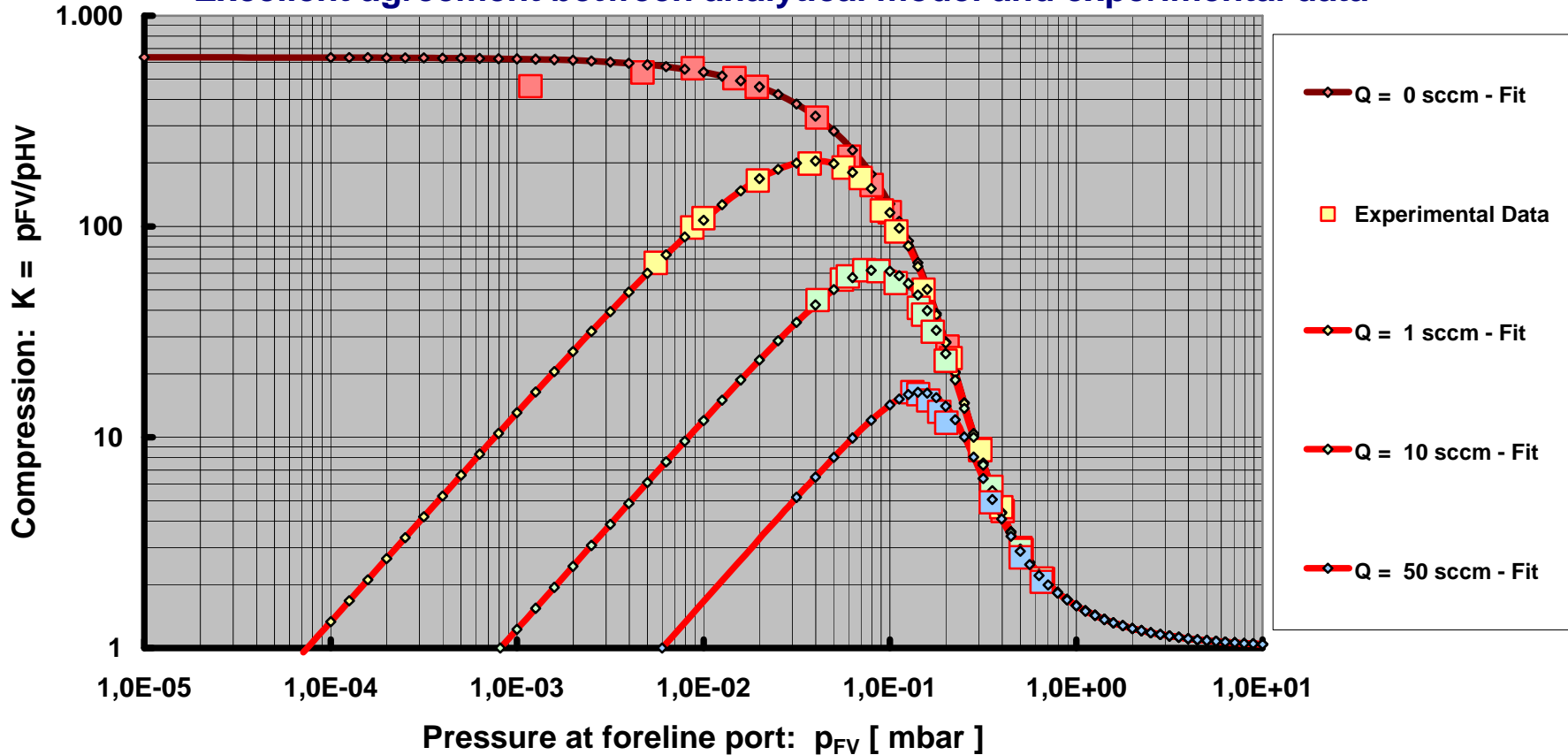


**TMP without compound stage (100 ISO-K; Rotational speed: 750 Hz)**

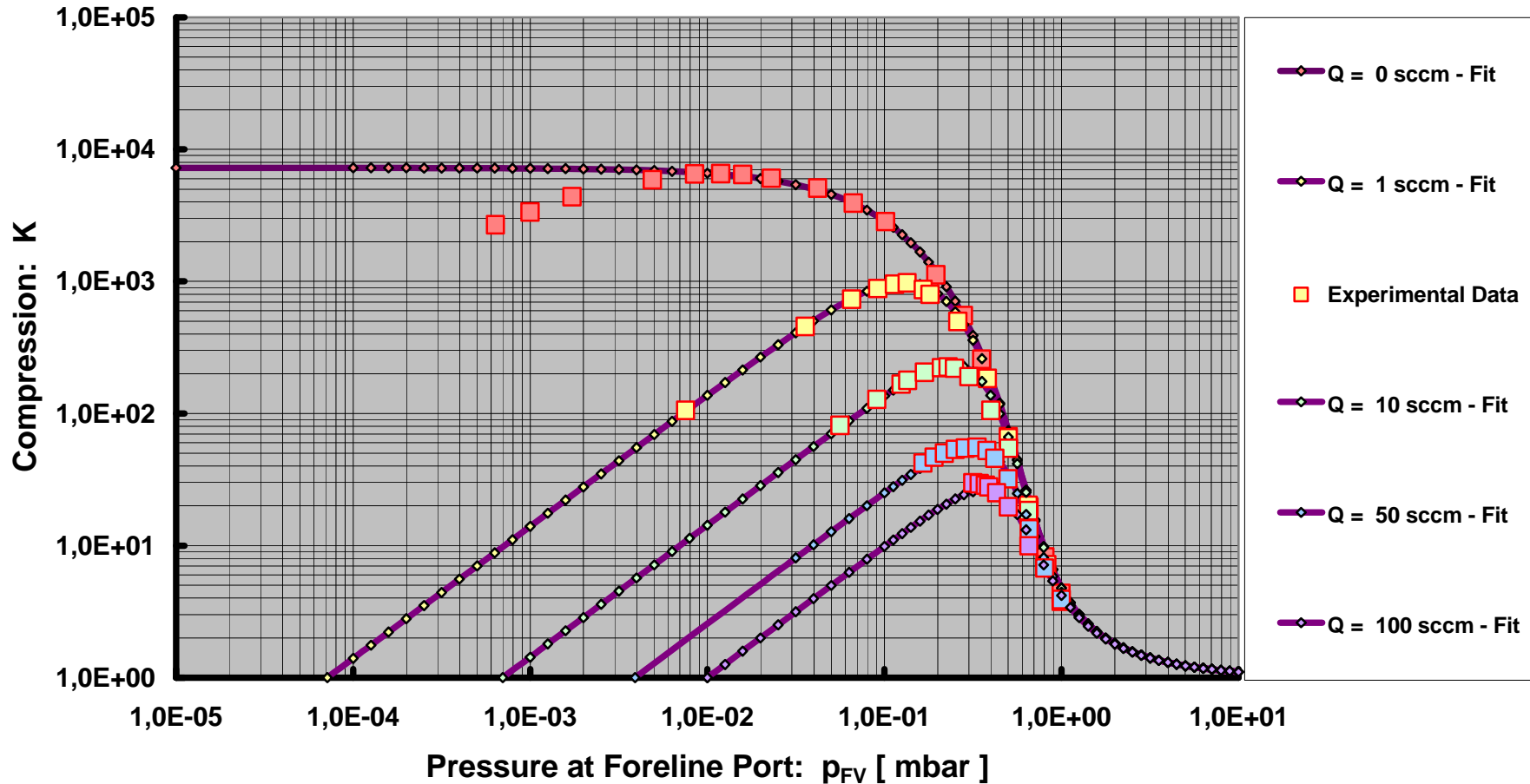
**Compression - Hydrogen**

(  $p_2 = 6,2 \times 10^{-2}$  mbar,  $C_2 = 0,4$  mbar,  $k_0 = \exp(C_2/p_2) = 634$  )

**Excellent agreement between analytical model and experimental data**



## TMP w/o Compound Stage (100 ISO-K; Rotational Speed: 750 Hz) Compression - Helium



## How to calculate the compression curve of a wide range turbomolecular pump ?

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Wide range turbomolecular pump (TMP) =  
Classical TMP plus compound stage

**Apply the analytical model twice !**

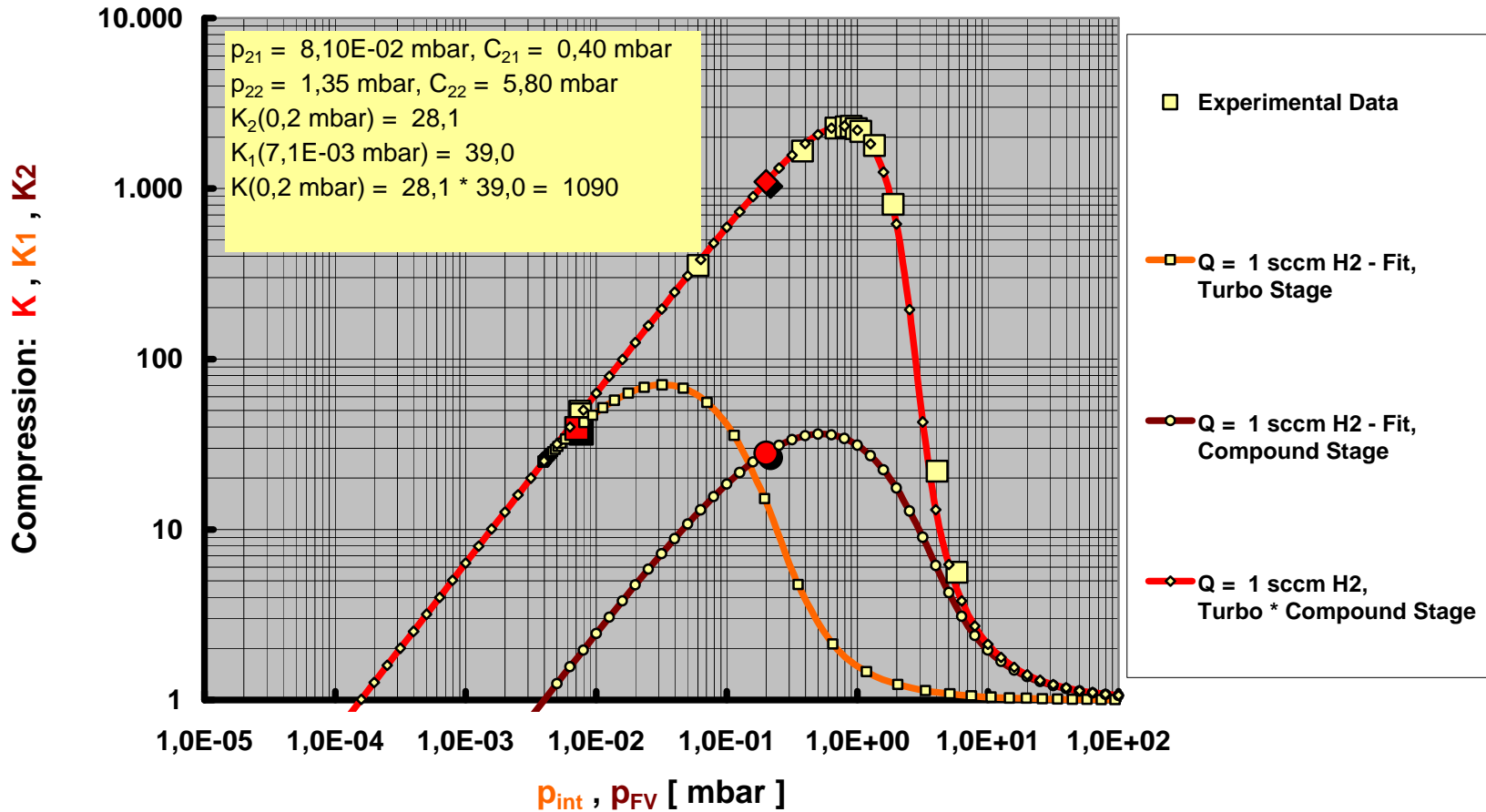
Turbo stage:           compression from  $p_{HV}$  to intermediate pressure  $p_{int}$   
 $K_1 = p_{int} / p_{HV}$

Compound stage:   compression from intermediate pressure  $p_{int}$  to  $p_{FV}$   
 $K_2 = p_{FV} / p_{int}$

Total compression:  $K = K_1 \cdot K_2 = p_{FV} / p_{HV}$

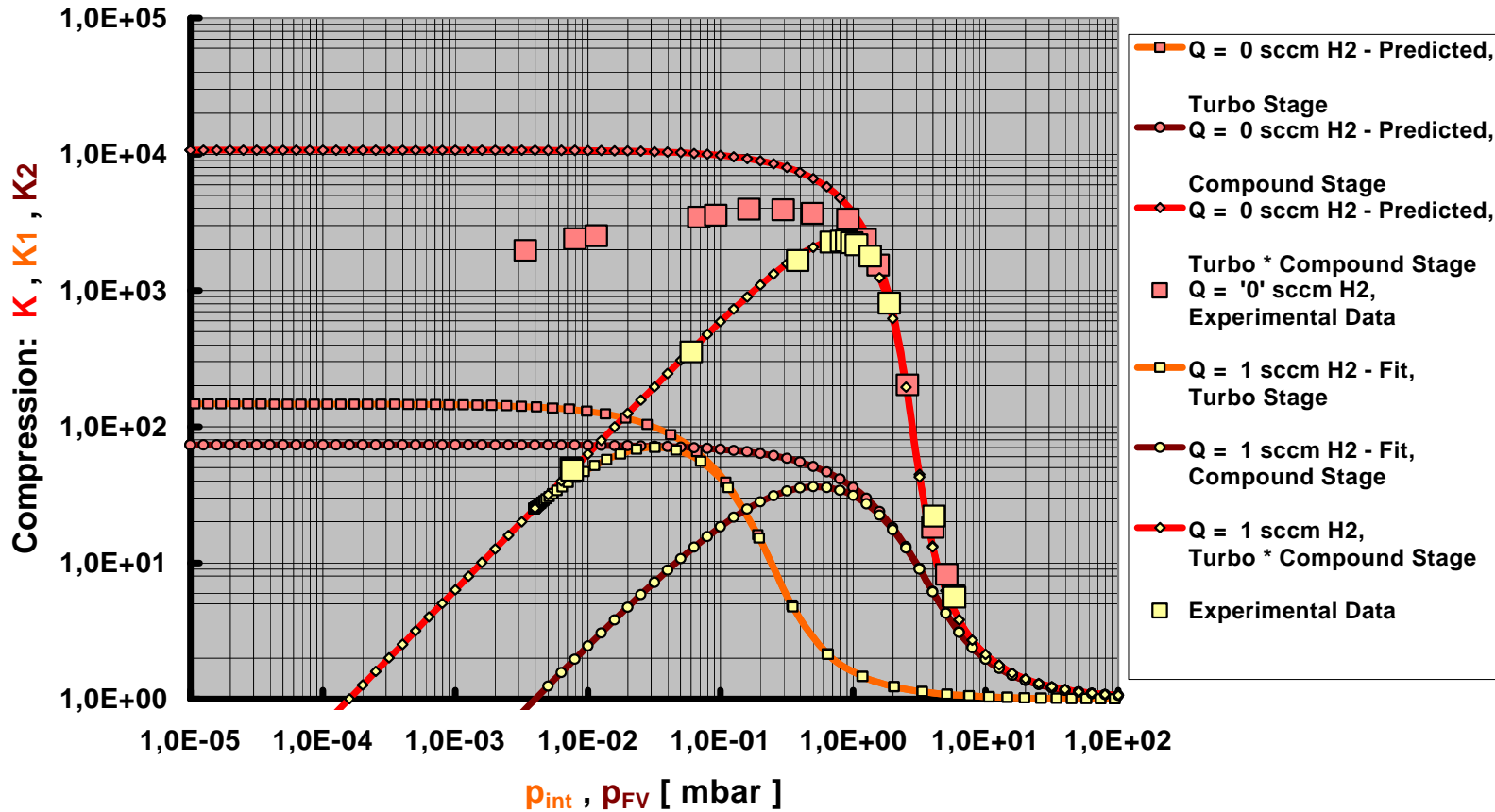
## TMP with Compound Stage (100 ISO-K; Rotational Speed: 1000 Hz) Compression - Hydrogen

The separation of turbo and compound stage works.

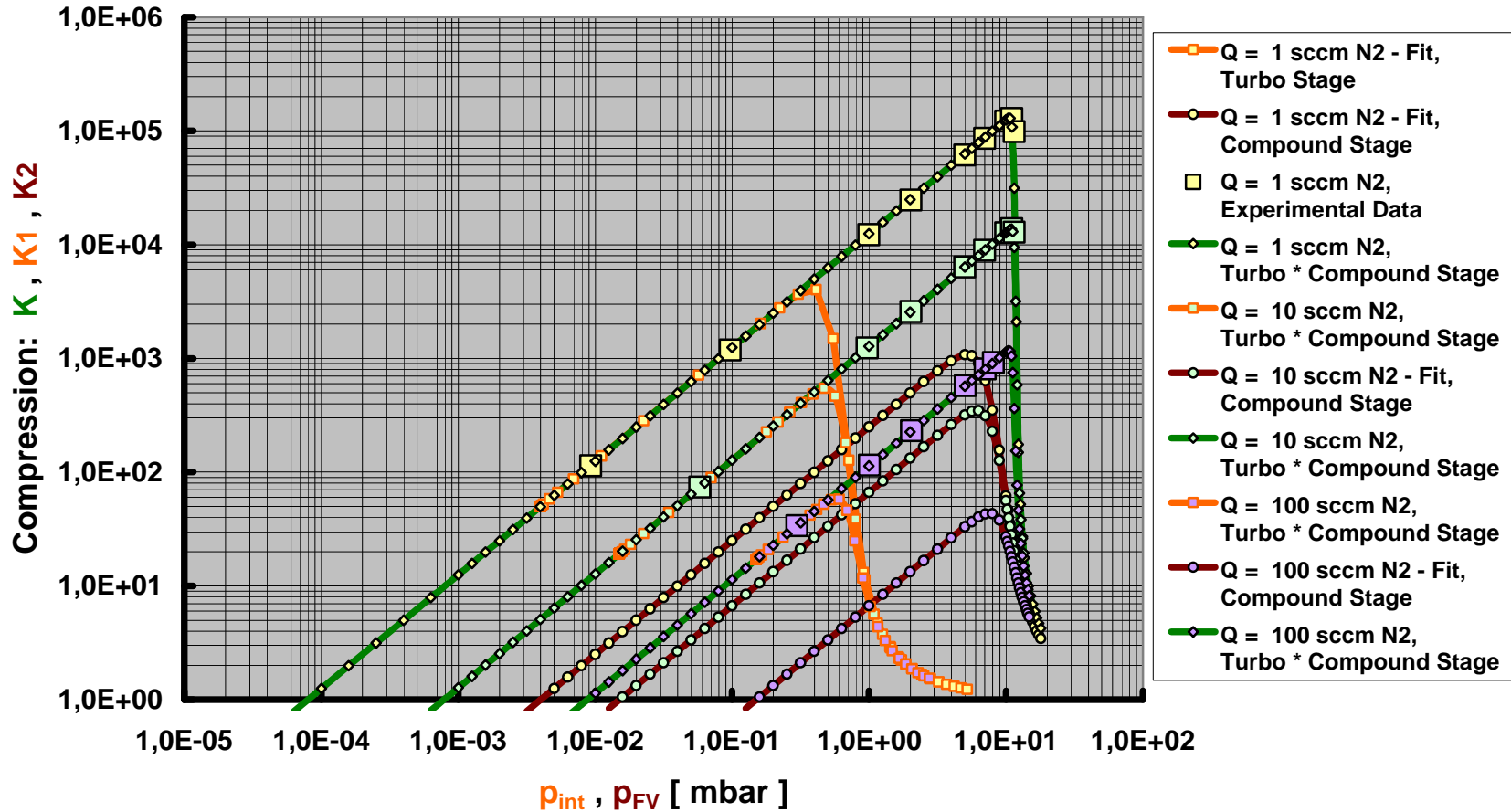


**TMP with Compound Stage (100 ISO-K; Rotational Speed: 1000 Hz)**  
**Compression - Hydrogen**

The true zero-throughput compression curves can be calculated.

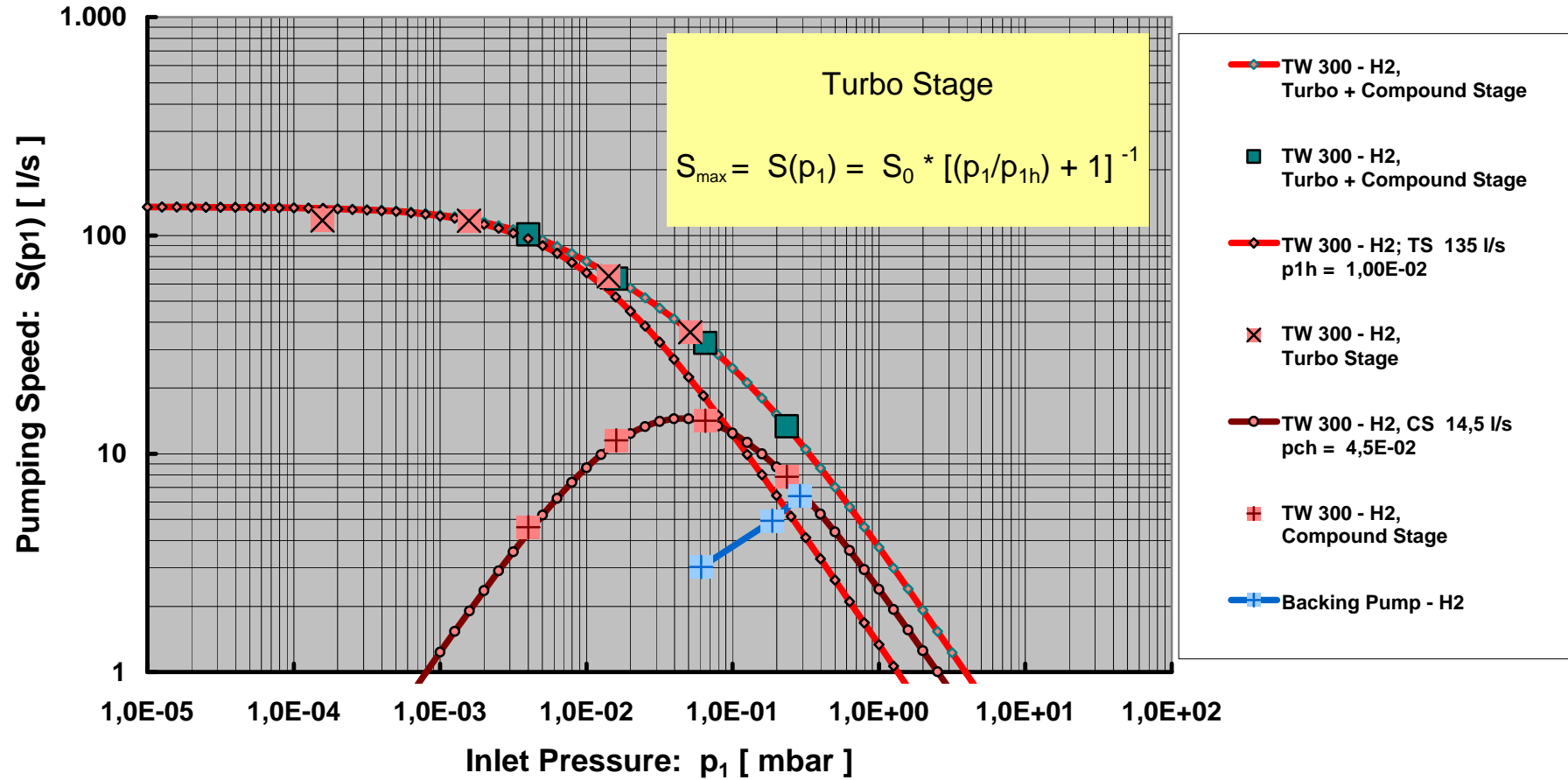


## TMP with Compound Stage (100 ISO-K; Rotational Speed: 1000 Hz) Compression - Nitrogen

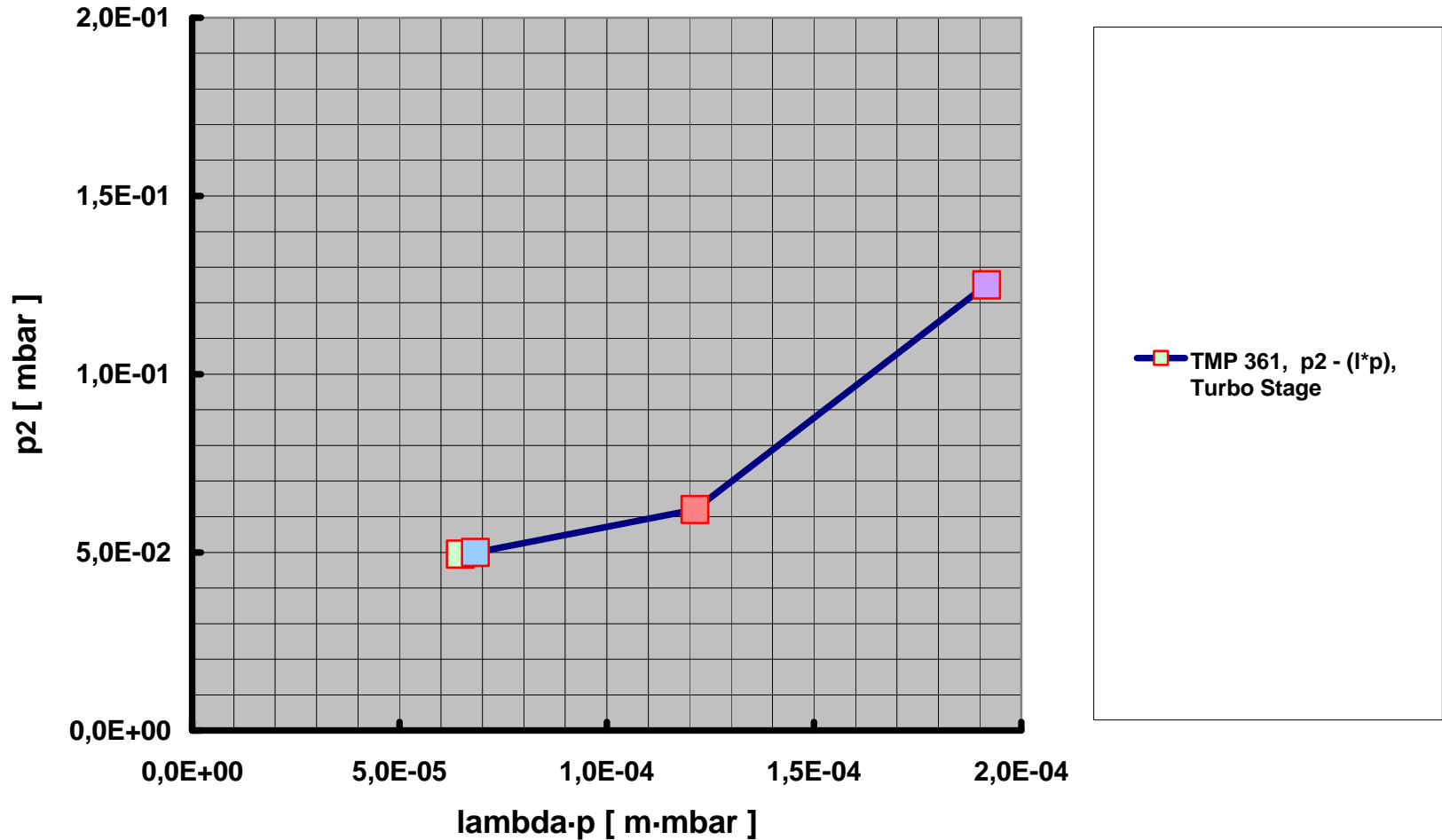




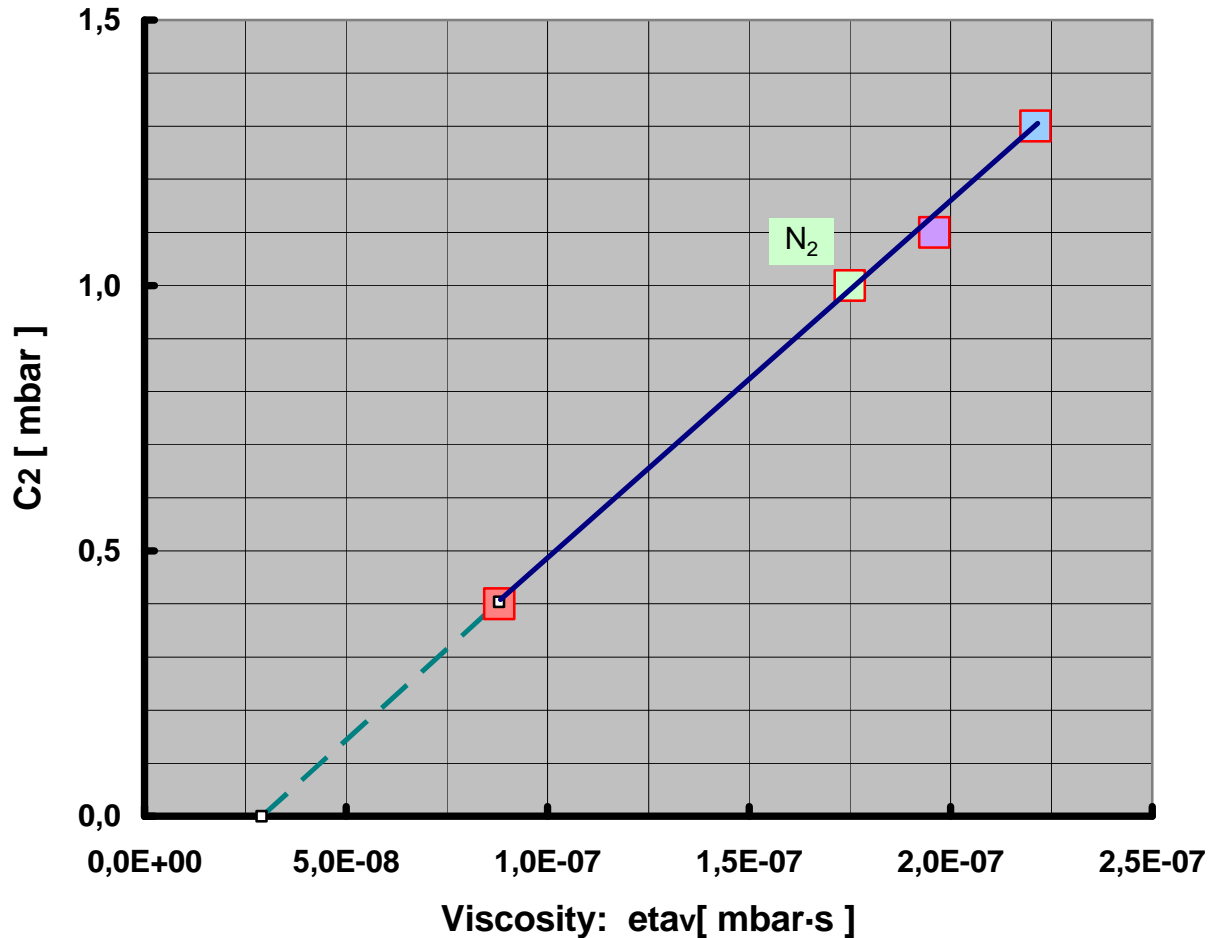
## TMP with Compound Stage (100 ISO-K; Rotational Speed: 1000 Hz) Pumping Speed for Hydrogen Turbo Stage and Compound Stage



## $p_2$ is a nonlinear function of $\lambda \cdot p$ !

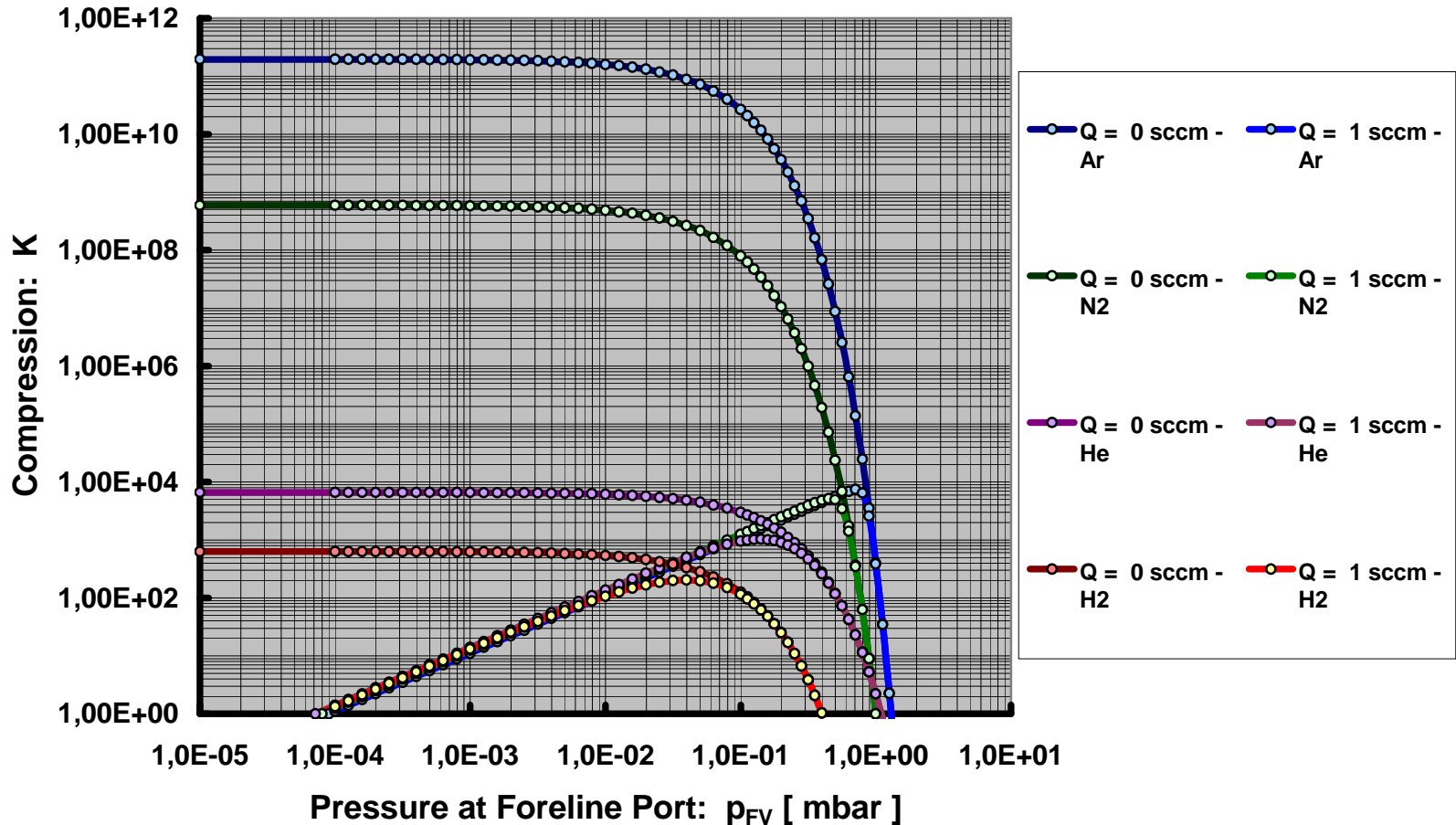


**There is a strong correlation between  $C_2$  and viscosity !**

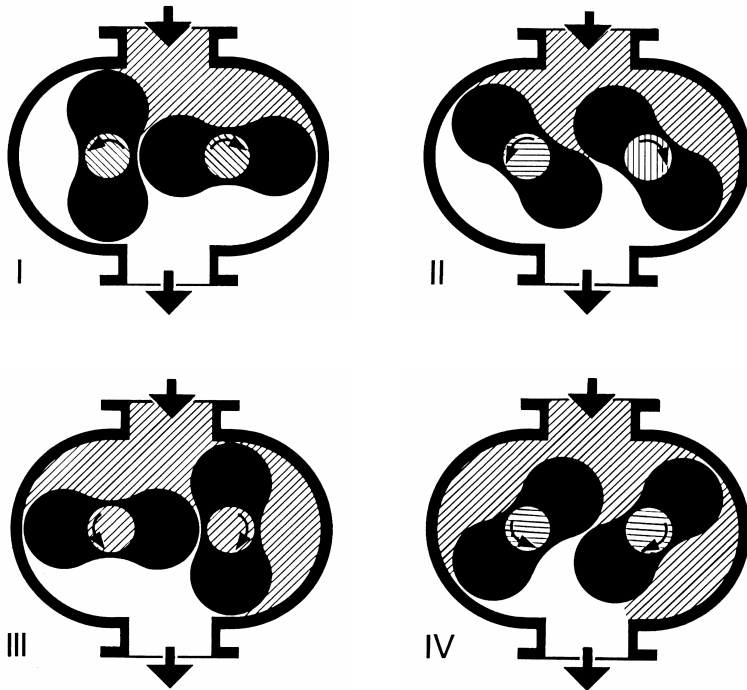


■ TMP 361, C2 - eta v,  
Turbo Stage

## TMP w/o Compound Stage (100 ISO-K; Rotational Speed: 750 Hz) Compression - Hydrogen, Helium, Nitrogen, Argon



# Principle of Roots Operation



- Two impellers rotate past each other in close proximity.
- In impeller positions **I** and **II**, the volume in the intake flange is increased.
- In position **III**, part of the volume is sealed off from the intake side.
- In position **IV**, this volume is opened to the discharge side.
- As the impellers rotate further, the compressed gas is ejected via the discharge flange.

## How to calculate the compression curve of a Roots blower ?

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**Use the same mathematical formalism as shown above in case of turbomolecular pumps !**

### **Analytical model:**

Roots blower (RB) in one dimension:

$x = 0$  : High-vacuum flange ( = inlet flange)

$x = L$  : Foreline port;  $L$  is taken as the effective length of the Roots blower

## Basic assumptions

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Ansatz:

$$Q = Q_{\max} - Q_{bs} - Q_{bl}$$

Net gas throughput = Maximum gas throughput in forward direction - Backstreaming - Backleakage

$$p_1 \cdot S_{\max} = p_{HV} \cdot S_{\max} - r \cdot (1/h_v) \cdot (p + p_2) \cdot (dp/dx) - p_{FV} \cdot S_{bl}$$

$h_v$  : Dynamic viscosity in the range of viscous flow

$p_2$  : Empirical parameter (depends on the geometry of the Roots blower)  
{  $p_2 = p_2(Q)$  }

## Backleakage in Roots blowers

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$$Q_{bl} = p_{FV} \cdot S_{bl} = \text{Backleakage}$$

$S_{bl}$  : Volume flow rate of gas transported by the rotors from the fore-vacuum side to the high-vacuum side, adsorption of gas on the fore-vacuum side – desorption of gas on the high-vacuum side, depends on foreline pressure

$p_{FV}$  : Foreline pressure

$p_{HV}$  : High-vacuum pressure



## Differential equation

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Differential equation:  $(r/h_v) \cdot (p + p_2) \cdot (dp/dx) = (p_{HV} - p_1) \cdot S_{max} - p_{FV} \cdot S_{bl}$

Boundary condition:  $p(x = 0) = p_{HV}$  (= high-vacuum pressure)

- x** : Position inside the RB  $\{ 0 \leq x \leq L \}$
- p** : Pressure inside the RB  $\{ p(x = 0) = p_{HV} \leq p = p(x) \leq p_{FV} = p(x = L) \}$
- p<sub>1</sub>** : Lowest high-vacuum pressure which can be attained with the RB  
at the prescribed gas throughput Q  $\{ p_1 = p_1(Q) \}$
- h<sub>v</sub>** : Dynamic viscosity in the range of viscous flow
- S<sub>max</sub>** : Maximum pumping speed at the inlet flange  
at the prescribed gas throughput Q  $\{ S_{max} = Q/p_1 = S(p_1) \}$
- r** : Backstreaming coefficient  $\{ r = r(Q) \}$

## Solution of the differential equation

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**First step: Neglect backleakage ( $S_{bl} = 0$ )**

Then the solution of the differential equation is:

$$p(x) = +[ (p_{HV} + p_2)^2 + 2 \cdot (p_{HV} - p_1) \cdot C_2 \cdot (x/L) ]^{1/2} - p_2$$
$$C_2 = h_v \cdot S_{max} \cdot L/r$$

$p_2$  and  $C_2$  are the crucial parameters of the model.

## High-vacuum pressure vs. foreline pressure

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$$p(x = L) = p_{FV} = +[ (p_{HV} + p_2)^2 + 2 \cdot (p_{HV} - p_1) \cdot C_2 ]^{1/2} - p_2$$

$$\textcircled{P} \quad (p_{HV} + p_2 + C_2)^2 = (p_{FV} + p_2 + C_2)^2 - 2 \cdot (p_{FV} - p_1) \cdot C_2$$

$$\textcircled{P} \quad (p_{HV} + p_2 + C_2)^2 - (p_{FV} + p_2)^2 = 2 \cdot (p_1 + p_2) \cdot C_2 + C_2^2$$

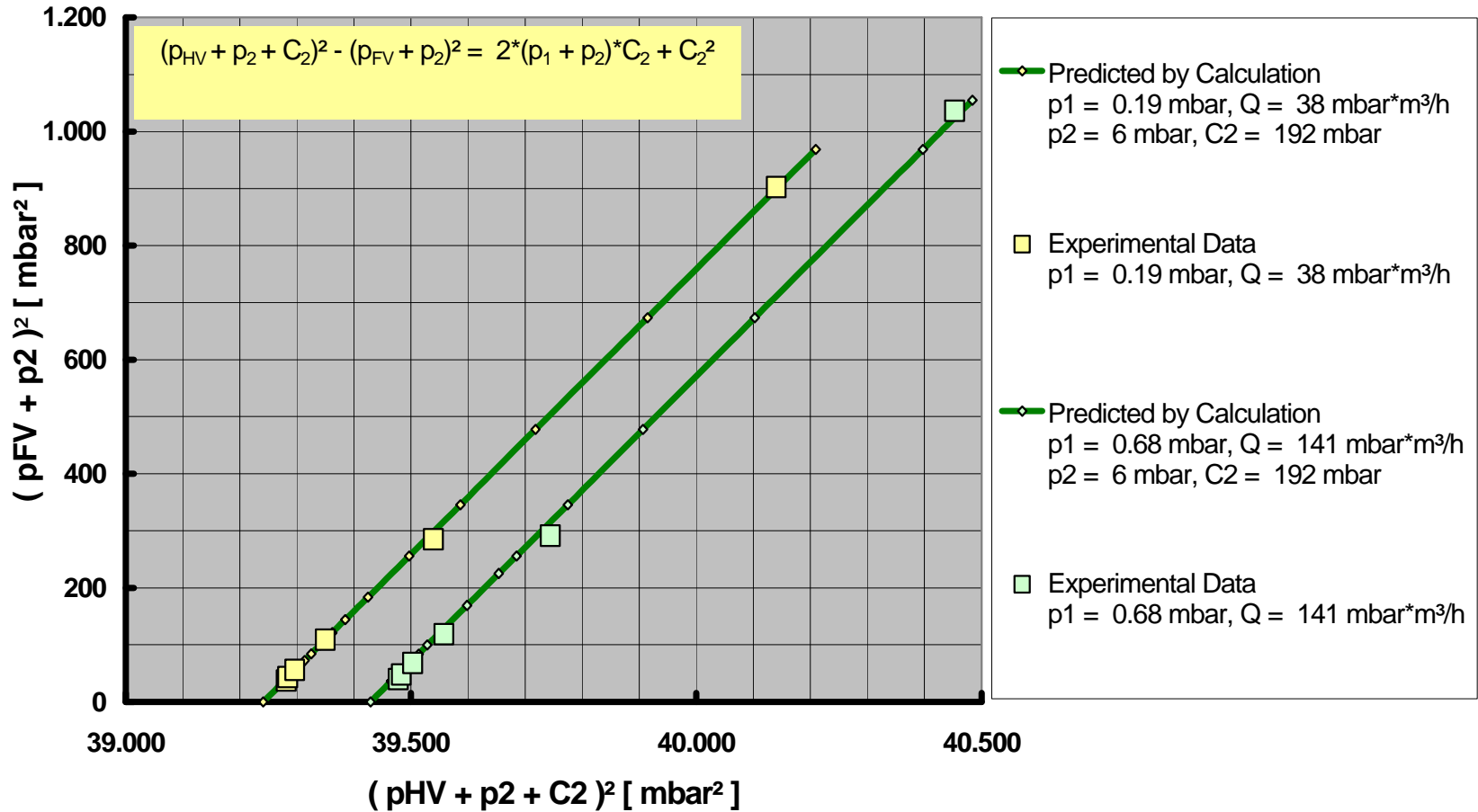
**High-vacuum pressure and foreline pressure form a hyperbola !**

Asymptotic behaviour:

1.  $p_{FV} = p_1$        $\textcircled{P} \quad p_{HV} = p_{FV}$
2.  $p_{FV} \gg C_2$        $\textcircled{P} \quad p_{HV} = p_{FV} - C_2$

## RuVac WA 251 + ScrewLine SP 630

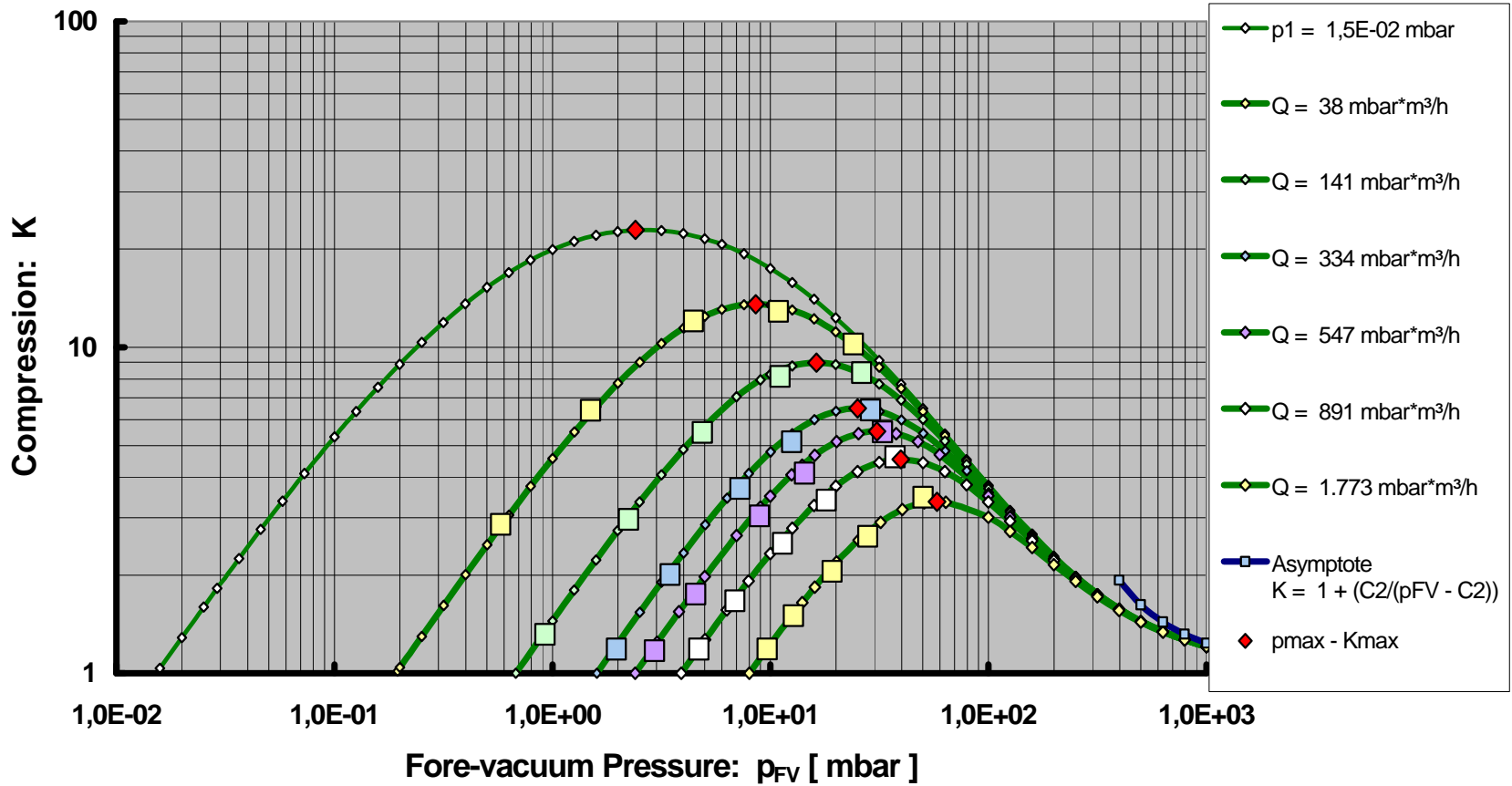
$p_{HV}$  and  $p_{FV}$  form a hyperbola



## RuVac WA 251 + ScrewLine SP 630 (50 Hz)

### Compression for Air

$p_2 = 6 \text{ mbar}$ ,  $C_2 = 192 \text{ mbar}$ ,  $S_{bl,0}/S_{max} = 0.02$ ,  $p_{bl} = 0.165 \text{ mbar}$



## Intuition

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The analysis of the compression curves leads to the following intuition:

- Ⓓ **One pair of parameters ( $p_2$ ,  $C_2$ ) can be used for all throughputs.**
- Ⓓ  **$C_2 = h_v \cdot S_{\max} \cdot L/r$  does not depend on throughput.**
- Ⓓ **Consequently,  $S_{\max}/r$  does not depend on throughput.**

## Compression vs. foreline pressure

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$$\text{Compression} = K = K(p_{FV}) = p_{FV}/p_{HV}$$

Asymptotic behaviour:

1.  $p_{FV} = p_1 \quad \Rightarrow \quad K = 1$
2.  $p_{FV} \gg C_2 \quad \Rightarrow \quad K = 1 + [ C_2/(p_{FV} - C_2) ]$

At prescribed gas throughput  $Q = p_1 \cdot S_{\max}(p_1)$  the maximum of the compression occurs at the following foreline pressure:

$$p_{FV, K_{\max}} = p_{\max} = [ 2 \cdot p_1 \cdot p_2 + (p_2 + C_2) \cdot (2 \cdot p_1 \cdot y)^{1/2} ] / (2 \cdot p_2 + C_2)$$

$$@ [ 2 \cdot p_1 \cdot (2 \cdot p_2 + C_2) ]^{1/2}$$

$$y = 2 \cdot (p_1 + p_2) + C_2$$

## Zero throughput compression

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$$Q = 0$$

$$\text{D} \quad (p_{HV} + p_2 + C_2)^2 = (p_{FV} + p_2 + C_2)^2 - 2 \cdot p_{FV} \cdot C_2$$

In the limit  $p_{FV} \ll p_2$  we obtain for the zero throughput compression:

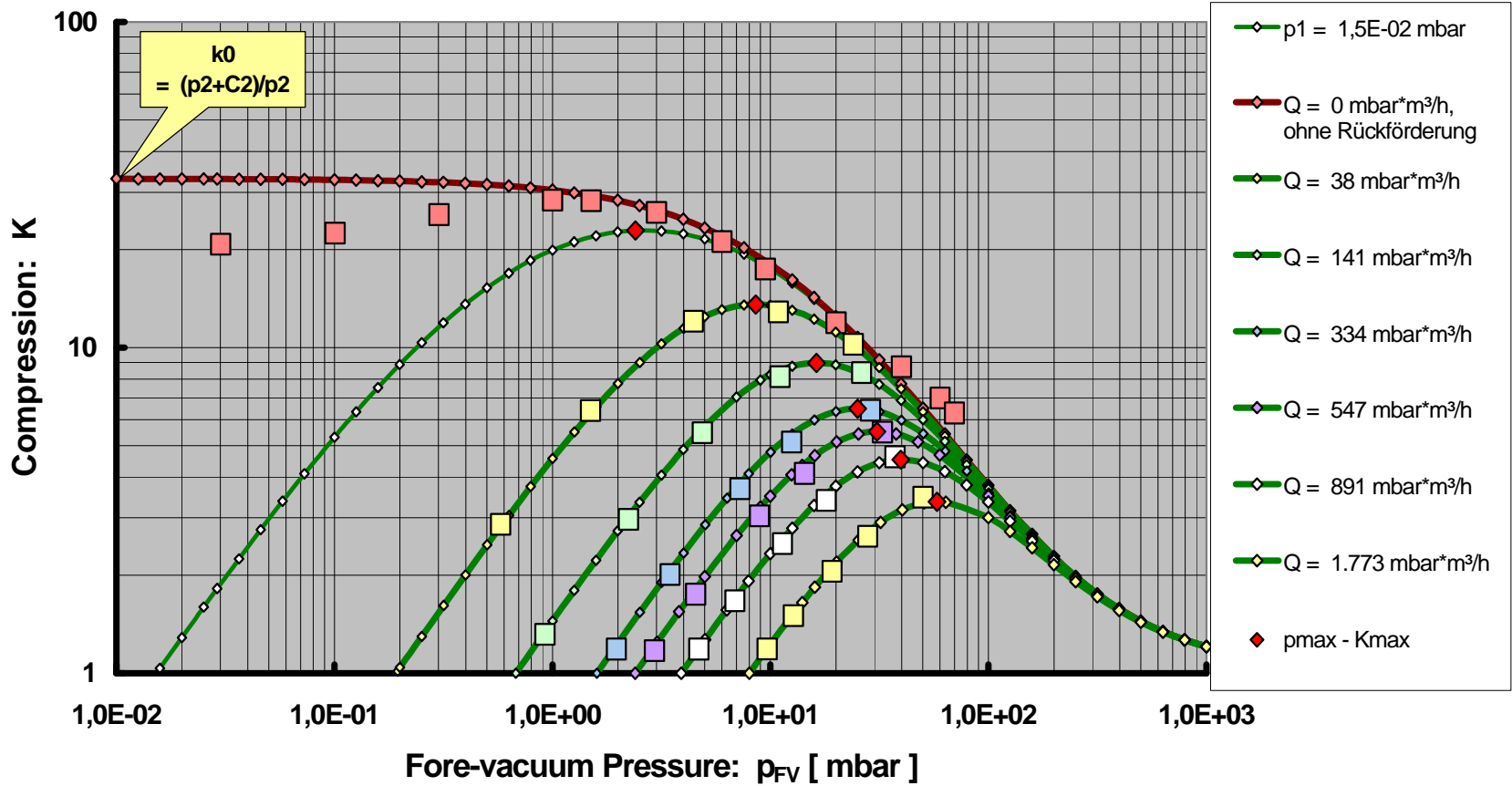
$$\text{D} \quad K_0 \text{ (R)} \quad k_0 = (p_2 + C_2)/p_2$$



## RuVac WA 251 + ScrewLine SP 630 (50 Hz)

### Compression for Air

$p_2 = 6 \text{ mbar}$ ,  $C_2 = 192 \text{ mbar}$ ,  $S_{bl,0}/S_{max} = 0.02$ ,  $p_{bl} = 0.165 \text{ mbar}$



## Zero throughput compression taking backleakage into account

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Substitute  $p_1$  by  $p_1 + [ (p_{FV} * S_{bl}(p_{FV})) / S_{max} ] !$

The Ansatz

$$S_{bl}(p_{FV}) = S_{bl,0} \cdot [ p_{bl} / (p_{bl} + p_{FV}) ]$$

leads to excellent agreement with the experiment.

$$p_{FV} \cdot S_{bl}(p_{FV}) \quad \textcircled{R} \quad p_{FV} \cdot S_{bl,0} \quad \text{for } p_{FV} \ll p_{bl}$$

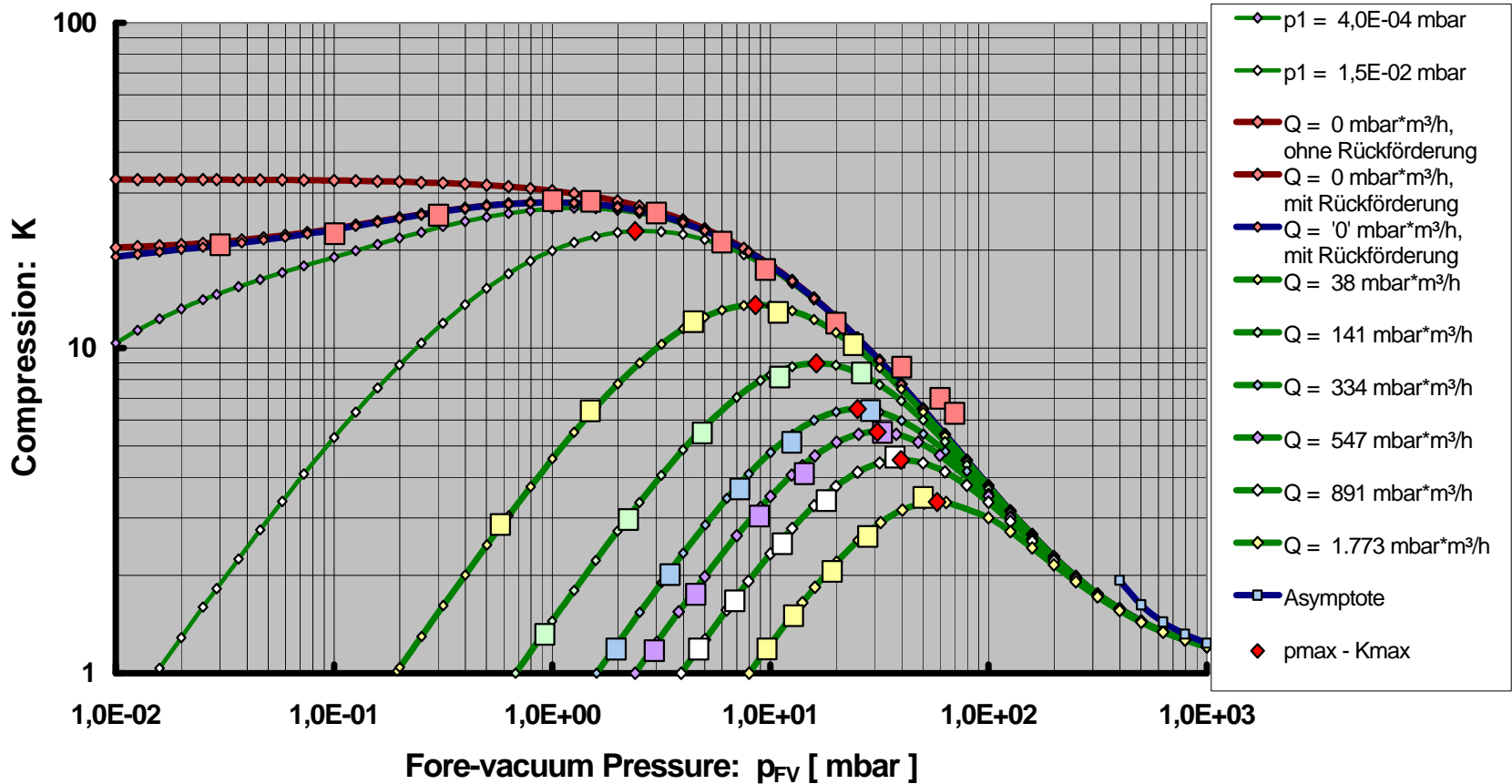
$$\quad \textcircled{R} \quad p_{bl} \cdot S_{bl,0} \quad \text{for } p_{FV} \gg p_{bl}$$

$$K_0 \quad \textcircled{R} \quad k_{0,bl} = (p_2 + C_2) / [ p_2 + C_2 \cdot (S_{bl,0} / S_{max}) ]$$

## RuVac WA 251 + ScrewLine SP 630 (50 Hz)

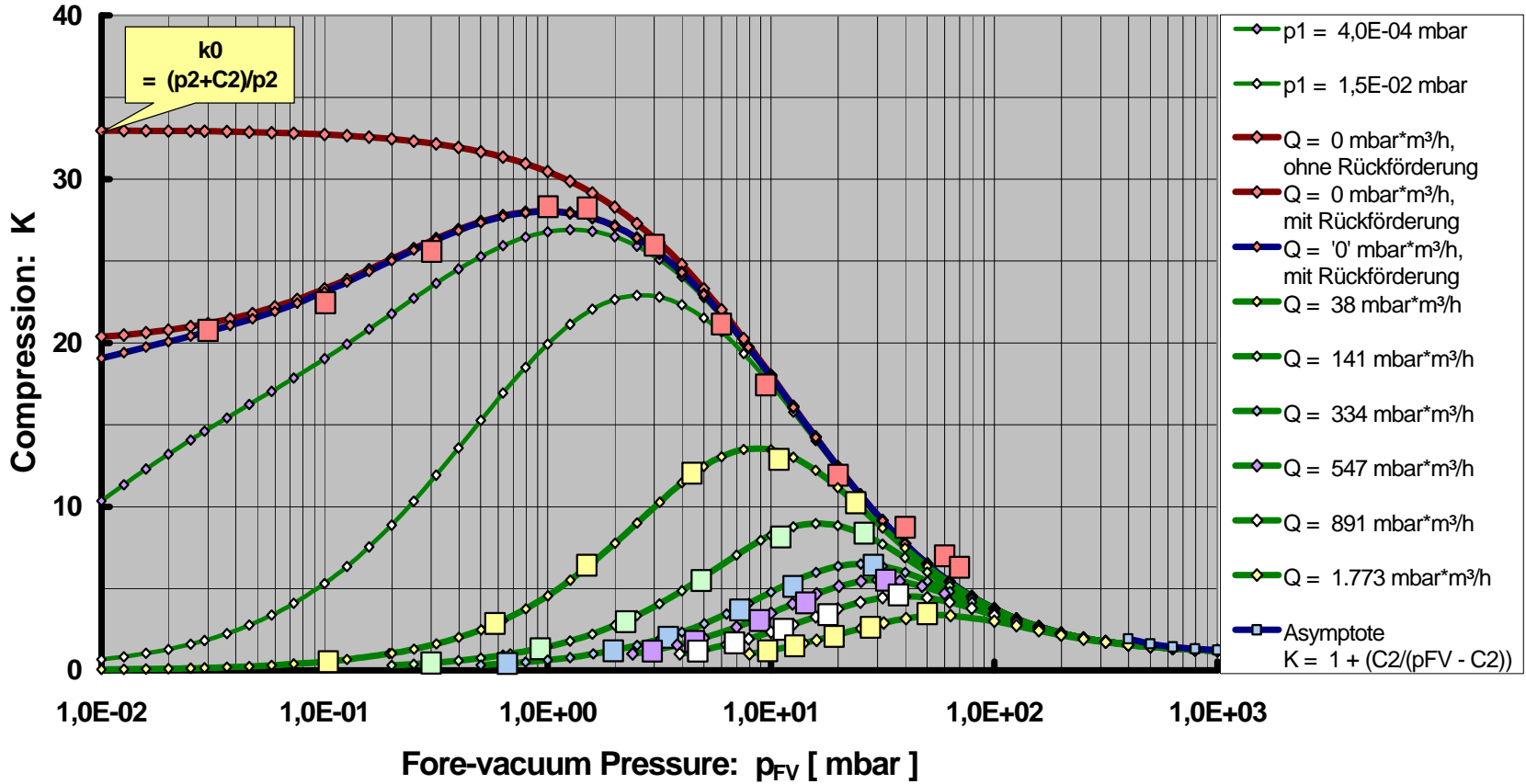
### Compression for Air

$p_2 = 6 \text{ mbar}$ ,  $C_2 = 192 \text{ mbar}$ ,  $S_{bl,0}/S_{max} = 0.02$ ,  $p_{bl} = 0.165 \text{ mbar}$



## RuVac WA 251 + ScrewLine SP 630 (50 Hz) Compression for Air

$p_2 = 6 \text{ mbar}$ ,  $C_2 = 192 \text{ mbar}$ ,  $S_{bl,0}/S_{max} = 0.02$ ,  $p_{bl} = 0.165 \text{ mbar}$



## The conductance of a Roots blower

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Using the analytical results of the model the following expression for the conductance can be derived:

$$C = [ S_{\max}/(2 \cdot C_2) ] \cdot (p_{HV} + p_{FV} + 2 \cdot p_2)$$

Note that

$$C_{\text{molecular}} = (p_2/C_2) \cdot S_{\max} = S_{\max}/(k_0 - 1)$$

can be taken as the conductance of the Roots blower in the range of molecular flow.

$$C = C_{\text{molecular}} \cdot [ 1 + (p_{HV} + p_{FV})/(2 \cdot p_2) ]$$

## On the compression in turbomolecular pumps and Roots blowers

### Summary

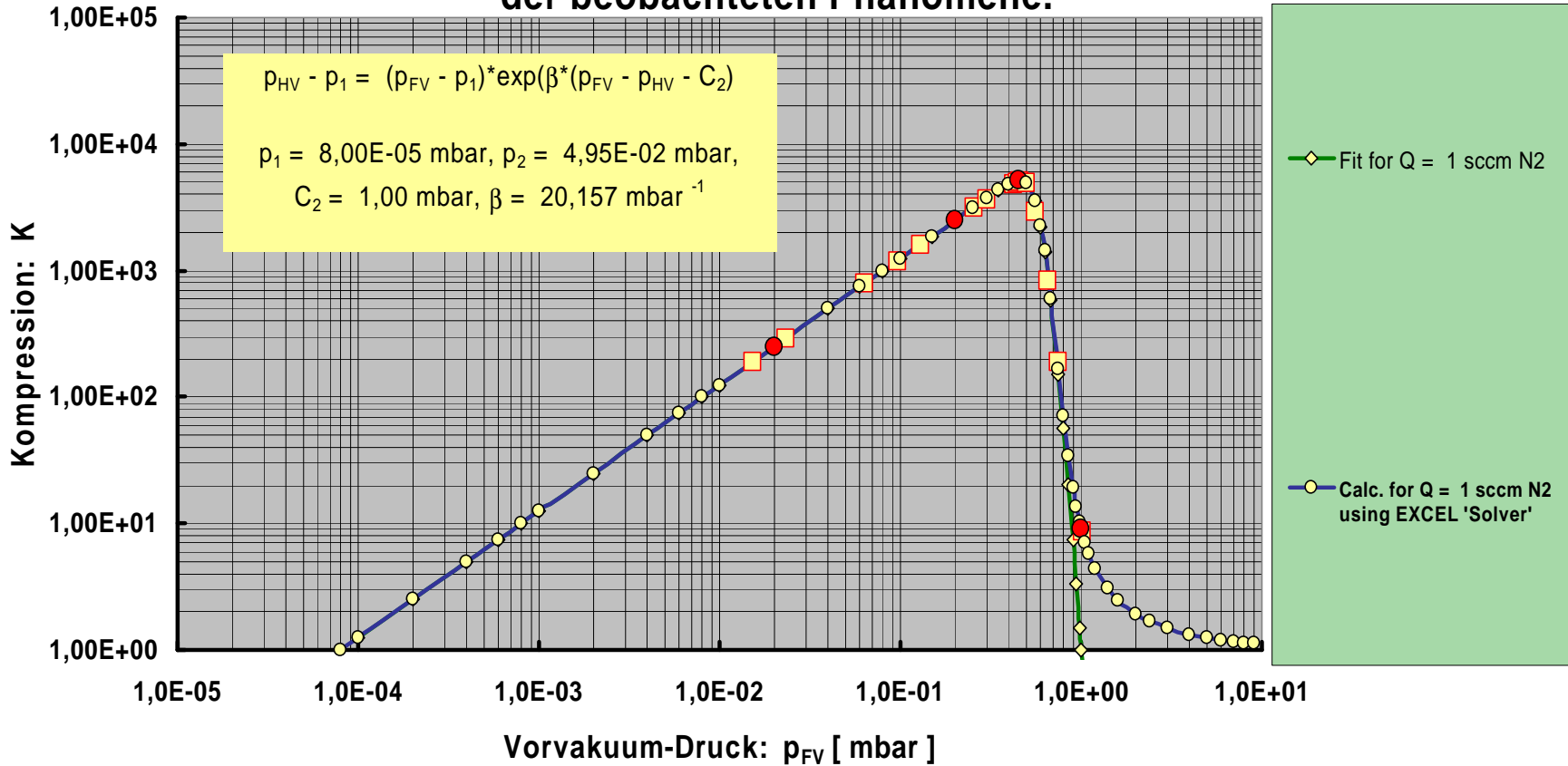
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- An analytical model has been presented for calculating and systematically analysing the compression curves for turbomolecular pumps, Wide Range turbomolecular pumps and Roots blowers.
  - Analytical expressions for the compression at finite ( $Q > 0$ ) and at zero throughput ( $Q = 0$ ) are provided by the model.
  - Only three parameters ( $p_1$ ,  $p_2$ ,  $C_2$ ) are required to describe the performance of a classical turbo stage, a compound stage or a Roots blower stage.
- There is strong evidence, that that the compression curve for zero gas throughput can be derived from a compression curve for a finite gas throughput.
- Comparison with experimental data shows that the analytical model provides an excellent qualitative and quantitative description of the observed phenomena.

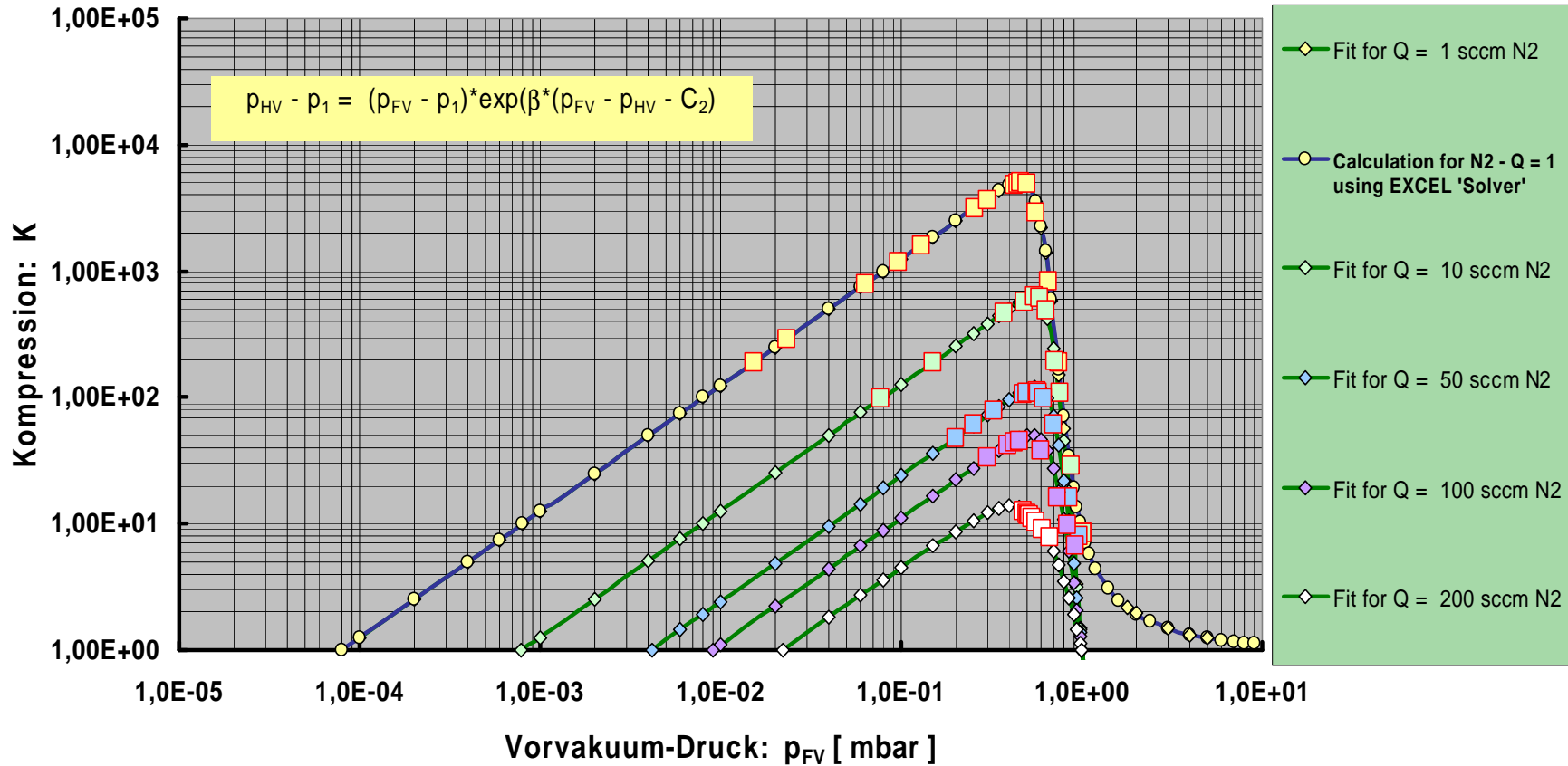
**Klassische TMP (100 ISO-K; 16 KF; Drehzahl: 750 Hz)**

**Kompression für Stickstoff**

**Das Modell liefert eine exzellente quantitative Beschreibung der beobachteten Phänomene.**

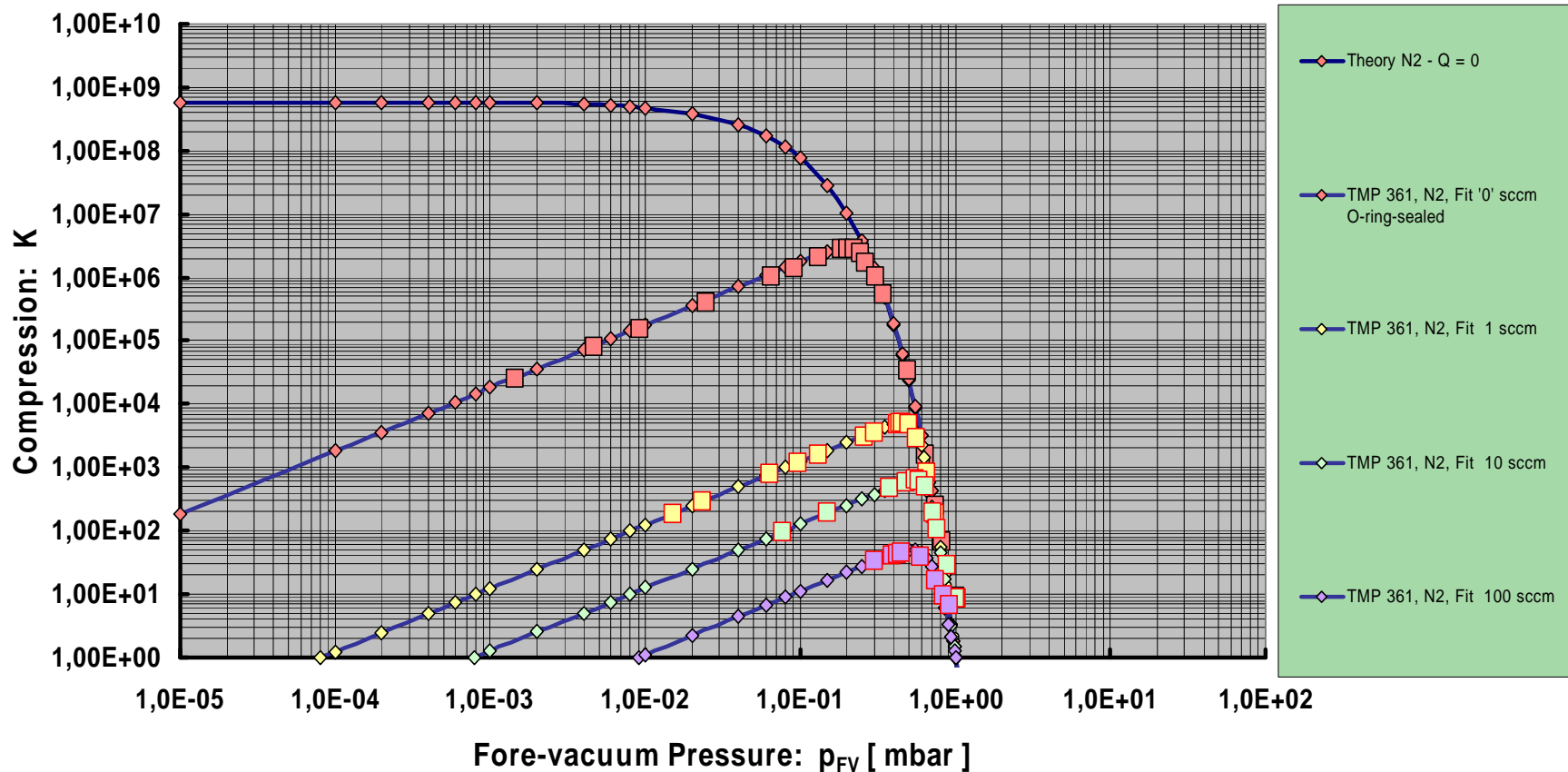


## Klassische TMP (100 ISO-K; 16 KF; Drehzahl: 750 Hz) Kompression für Stickstoff



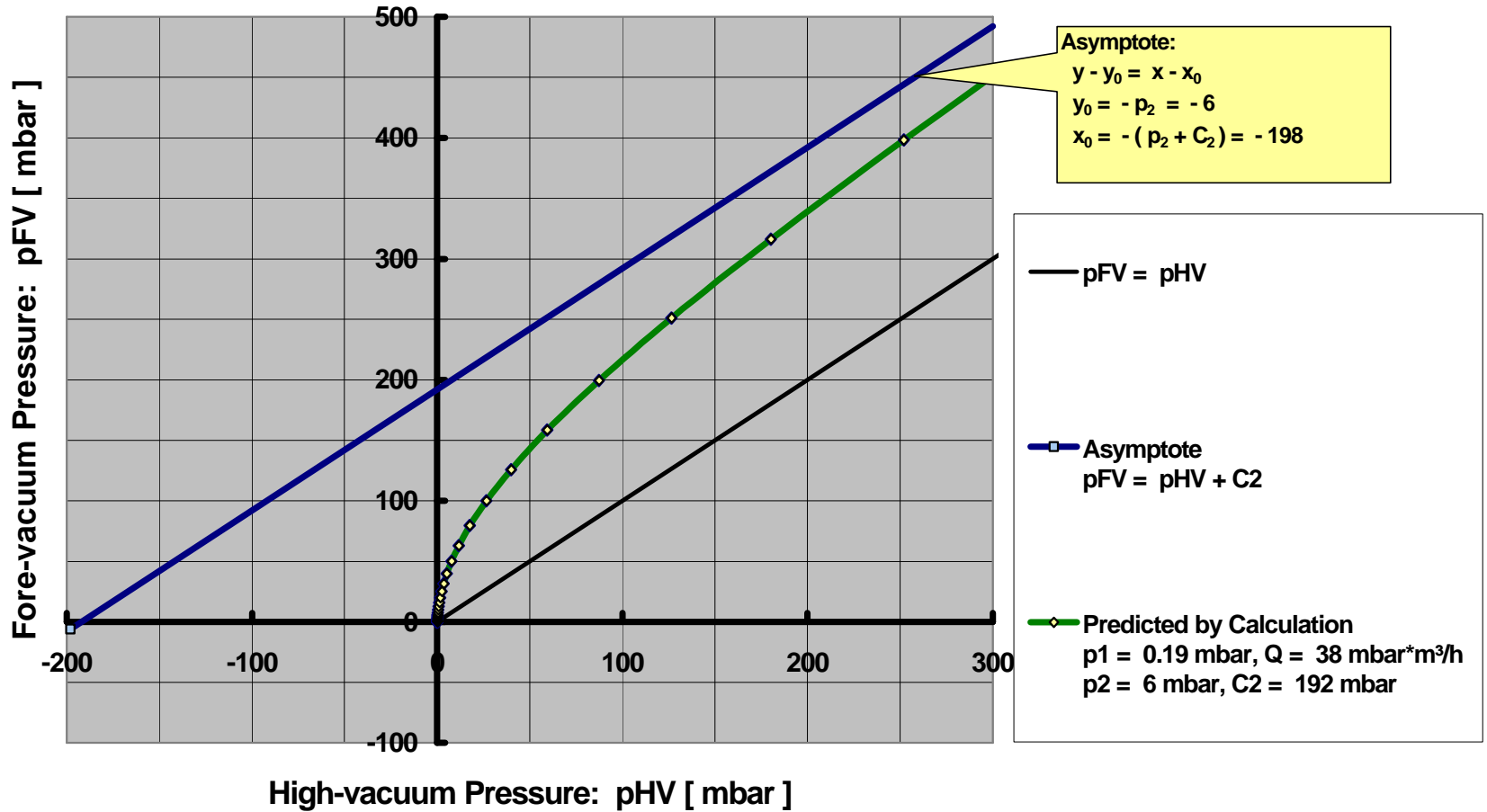


## Classic TMP (100 ISO-K; 16 KF) Compression for Nitrogen



## RuVac WA 251 + ScrewLine SP 630

$p_{HV}$  and  $p_{FV}$  form a hyperbola



## TMP with Compound Stage (100 ISO-K; Rotational Speed: 1000 Hz) Pumping Speed for Nitrogen, Helium and Hydrogen Turbo Stage and Compound Stage

